## Amendment to the Claims

This listing of claims will replace all prior versions and listings of claims in the application:

## **Listing of Claims:**

 (Original) A method of main reformer startup, comprising: introducing a first supply of fuel and a first supply of air into a micro-reformer;

increasing said first supply of fuel to produce a heated reformate in said micro-reformer;

directing said heated reformate through a main reformer to heat said main reformer;

burning at least a portion of said heated reformate in said main reformer; and

introducing a second supply of fuel and a second supply of air to said main reformer to produce a main supply of reformate.

- 2. (Original) The method of Claim 1, further comprising electrically preheating said micro-reformer.
- 3. (Original) The method of Claim 2, wherein said micro-reformer has an inlet air temperature at about 140°C or greater and a catalyst exit temperature of about 300°C or greater.

- 4. (Original) The method of claim 1, wherein said micro-reformer has a
- catalyst volume of about 50% or less of a catalyst volume of said main reformer.
- (Original) The method of Claim 1, wherein said main reformer
- consists essentially of a catalyst and ceramic components.
- 6. (Original) The method of Claim 1, wherein said first supply of fuel
- has an equivalence ratio of about 0.4 to about 0.7.
- 7. (Original) The method of Claim 1, wherein said increasing said first
- supply of fuel is to an equivalence ratio of about 2.7 to about 2.9.
- 8. (Original) The method of Claim 7, wherein said micro-reformer has
- a catalyst exit temperature of about 500°C or greater.
  - 9. (Original) The method of Claim 1, wherein said second supply of
- fuel has an equivalence ratio of about 1.8 to about 2.2.
  - 10. (Original) The method of Claim 9, wherein said main reformer has
- catalyst exit temperature of about 500°C or greater.
  - 11. (Cancelled).

- 12. (Cancelled).
- 13. (Currently amended) The method of Claim 12 4, wherein said micro-reformer has a catalyst volume equal to about 35% or less of a catalyst volume of said main reformer.
- 14. (Currently amended) The method of Claim 12 4, wherein said micro-reformer has a catalyst volume equal to about 25% to about 10% of a catalyst volume of said main reformer.
- 15. (Withdrawn) A method for maintaining a vehicle device in standby condition, comprising:

introducing a supply of fuel and a supply of air into a micro-reformer; increasing said supply of fuel to produce a heated reformate in said micro-reformer;

passing at least a portion of said heated reformate through said vehicle device; and

maintaining said vehicle device at a standby temperature.

16. (Withdrawn) The method of Claim 15, further comprising electrically pre-heating said micro-reformer.

- 17. (Withdrawn) The method of Claim 16, wherein said micro-reformer has an inlet air temperature at about 140°C or greater and a catalyst exit temperature of about 300°C or greater.
- 18. (Withdrawn) The method of Claim 15, further comprising burning at least a portion of said heated reformate in said vehicle device.
- 19. (Withdrawn) The method of Claim 15, wherein said vehicle device is a device selected from the group consisting of a reformer, a waste energy recovery burner device, a catalytic after treatment system, a burner, a fuel fired heater device, and combinations comprising at least one of the foregoing devices.
- 20. (Withdrawn) The system of Claim 15, wherein said standby temperature is about 200°C to about 400°C.
- 21. (Withdrawn) The system of Claim 20, wherein said standby temperature is about 250°C to about 300°C.
- 22. (Withdrawn) The method of Claim 15, wherein said first supply of fuel has an equivalence ratio of about 0.4 to about 0.7.
- 23. (Withdrawn) The method of Claim 15, wherein said increasing said first supply of fuel is to an equivalence ratio of about 2.7 to about 2.9.

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24. (Withdrawn) The method of Claim 23, wherein said micro-reformer has a catalyst exit temperature of about 500°C or greater.

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